### MATHEMATIC MODEL FOR OPTIMIZATION OF ZINC-NICKEL ALLOY CO-DEPOSITION PROCESS

<sup>1</sup>Violeta VASILACHE, <sup>2</sup>Marius BENȚA

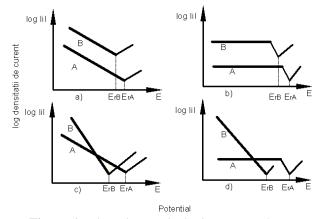
<sup>1</sup>Universitatea Ştefan cel Mare, Suceava, Str. Universității, Nr.13, 720229, Suceava, <u>violetav@fia.usv.ro</u> <sup>2</sup>Universitatea Transilvania Brasov, Bulevardul Eroilor, No.29, 500036, Brasov,

**Abstract:** Any optimization method implies a mathematical model which should resolve the quantitative requires of the problems. This model is based on the substrate effect and has to calculate the partial current densities and so has to give prediction as far as concern the quantities of metal electrodeposited and the energy involved.

**Keywords:** *mathematical model, anomalous co-deposition, zinc-nickel alloys, mass transfer, electrochemical kinetic* 

### **1. INTRODUCTION**

Electrodeposition of a simple metal has also a simplier mathematical model, but situation is different for alloys deposition. In our proposed model kinetic parameters are analyzed and it was made the supposition that current distribution and mass transport are homogeneous on working electrode. Also we tried to determinate the reaction mechanism.



**Figure 1.** The scheme which shows partial current densities for A and B components. (a) both components under activation kinetic control, present identic Tafel slopes. (b) both components present limitation of the current. (c) both components under activation control, but with different Tafel slopes. (d) component A presents current limitation, component B under activation control.

### 2. EXPERIMENTAL CONSIDERATIONS

### 2.1. Electrochemical processe at cathode

In our experiments it was deposited zinc-nickel alloy on gold substrate, previous deposited by sputtering on glass plates. This methode was chosen because it permits to analyze the layers with XRD and SEM-EDX techniques.

The mechanism of electrochemical reactions which occur on cathode surface has two steps, as Matlosz described Matlosz [4], [5]. Zinc ions are deposits on their own substrate, on gold substrate and on nickel substrate. Also nickel ions are deposited on their own substrate, on gold substrate and on zinc substrate. More, there are secondary reactions,  $Zn^{2+}$  ions are combining with hydrogen to form  $ZnH^+$ , and similar  $Ni^{2+}$  ions are combining to hydrogen to form  $NiH^+$ . These intermediate species, formed in adsorption process, finally will be decomposed to metallic zinc and nickel respectively.

The mechanism of electrochemical reactions could be written as follow:

$$Ni^{2+} + e^{-} \rightarrow Ni^{+}_{ads} \tag{1}$$

$$Ni^+_{ads} + e^- \rightarrow Ni$$
 (2)

$$Ni + H^+ + \rightarrow NiH^+_{ads} \tag{3}$$

$$NiH^{+}_{ads} + H^{+} + 2e^{-} \rightarrow Ni + H_2 \quad (4)$$

$$Zn^{2+} + e^{-} \rightarrow Zn^{+}_{ads} \tag{5}$$

$$Zn^+ + e^- \to Zn \tag{6}$$

$$Zn + H^+ \to ZnH^+_{ads} \tag{7}$$

$$ZnH^{+}_{ads} + H^{+} + 2e^{-} \rightarrow Zn + H_2 \qquad (8)$$

 $Ni^{2+}$  and  $Zn^{2+}$  are disolved as metallic ions, hydrolized or not.  $Ni^+_{ads}$  and  $Zn^+_{ads}$  which could contain or not the group hydroxyl are adsorbed in intermediate reactions. Ni and Zn are metallic deposits of nickel and zinc respectively [6,7]. The kinetic of mass transfer is supposed to respect Butler-Volmer equation. In far from equilibrium states anodic reactions could be neglected.

# 2.2. Determination of partial current densities

For a binary alloy AB and a thicknes of deposit  $\Delta d$ , partial current density of *B* element is,

$$i_B = \frac{n_B F}{m_B \Delta t} m_B \tag{9}$$

Here  $m_B$  is mass of element B deposited in alloy,  $M_B$  is atomic mass of element B,  $\Delta t$  is deposition time and  $n_B$  is number of electrons implied in reaction of element B.

# 2.3. Normal and anomalous co-deposition of zinc-nickel alloys

Electrodeposition of zinc-nickel alloys is generally an anomalous co-deposition, after Brenner's deffinition, because the metal less noble, zinc, is deposited preferential and its percent in deposit is higher than in electrolyte. Anyway, normal co-deposition of zinc-nickel alloys is possible only in particulary experimental conditions. Co-deposition of zinc-nickel alloys from different electrolytic bath was studied potentiostatic and galvanostatic, function of different variable parameters during the electrodeposition [1,2].

# 2.4. Mathematical modeling of zinc-nickel alloy co-deposition. The model of substrate effect

The initial nucleation of adsorbed nickel on electrode surface acts as a catalyser for zinc deposition, resulting an inhibition of nickel deposition. Also it was shown that pure zinc cannot be deposited from aqueous electrolyt solutions at UPD (*underpotential deposition*), but it could be co-deposited with nickel. These phenomena can be explaine by the fact that nickel nucleation catalize zinc deposition. At potential more negative than zinc equilibrium potential, zinc deposition rate is enough higher and inhibits nickel deposition resulting an anomalous co-deposition.

The alloy deposition performs uner substrate effect. Not only nickel affects zinc deposition, but zinc too affects nickel deposition.

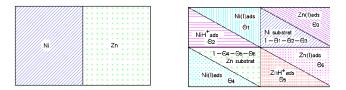


Figure 2. The diagram of zinc-nickel alloy co-deposition

In figure 2 is represented the diagram of the effects of different substrates during electroplating with zinc-nickel alloys. The initial electrode surface is divided in two parts. The first is corresponding to  $\theta_{Ni}$  which is the surface covered by nickel and the second is the surface covered by zinc,  $\theta_{Zn}$ . Every surface is then divided in four parts. So, for nickel deposition,  $\theta_{Ni}\theta_1$  corresponds to the area of Ni substrate surface covered with  $Ni(I)_{ads}$ .  $\theta_{Ni}\theta_2$  corresponds to the area of Ni substrate surface covered with substrate surface covered with  $NiH^+_{ads}$ ,  $\theta_{Ni}\theta_3$  corresponds to the area of Ni substrate surface covered with  $Zn(I)_{ads}$ . Free surface  $\theta_{Ni}(1-\theta_1-\theta_2-\theta_3)$  corresponds to the area of Ni substrate surface non-covered.

For zinc deposition,  $\theta_{Zn}\theta_6$  corresponds to the area of Zn substrate surface covered with  $Zn(I)_{ads}$ .  $\theta_{Zn}\theta_5$  corresponds to the area of Zn substrate surface covered with  $ZnH^+_{ads}$ .  $\theta_{Zn}\theta_4$ corresponds to the area of Zn substrate surface covered with  $Ni(I)_{ads}$ . Free surface  $\theta_{Zn}(1-\theta_4-\theta_5-\theta_6)$ corresponds to the area of Zn substrate surface non-covered.

# 2.5. Theoretic model. General mechanism of electrode reactions

A mechanism of reactions was developed as effect of substrate. his model is based on the supposition that every individual component is deposited after a two steps-reaction, as Matlosz [4] described. The nickel ions are deposited on their own substrate and on zinc substrate. Also zinc ions are deposited on their own substrate and on nickel substrate. More, hydrogenated species  $ZnH^+$  and  $NiH^+$  are strongly bonded at electrode surface. Ni(II) will react giving  $NiH^+_{ads}$  and these adsorbed species will react after with deposited nickel. Also Zn(II) will react giving  $ZnH^+_{ads}$  and these adsorbed species will react after with deposited zinc.

### 2.6. The mass transfer effect

The material balance in equilibrium state through diffusion layer for species Ni(II), Zn(II) and  $H^+$ , 0<x<d, can be written

$$\nabla \cdot N_{Ni(II)} = 0 \tag{10}$$

$$\nabla \cdot N_{Zn(II)} = 0 \tag{11}$$

$$\nabla \cdot N_{H^+} = 0 \tag{12}$$

$$K_{W} = C_{OH^{-}} \cdot C_{H^{+}} \tag{13}$$

Supposing a constant diffusion coefficient, *D*, the flow of every species *i*, into diffusion layer is  $N_i = -DdC_i/dx$ . Accepted values for diffusion coefficients are  $4 \times 10^{-10} m^2 s^{-1}$  for Ni(II),  $5,09 \times 10^{-10} m^2 s^{-1}$  for Zn(II), and  $9,3 \times 10^{-9} m^2 s^{-1}$  for solvated protons, and  $5,5 \times 10^{-9} m^2 s^{-1}$  for hydroxid ions [3]. Intermediate species,  $Ni(I)_{ads}$ ,  $NiH^+_{ads}$ ,  $Zn(I)_{ads}$  and  $ZnH^+_{ads}$  existe only on the electrode surface so one their concentration is equal zero in solution [8], [9].

#### 2.7. Electrochemical kinetic

The charge transfer kinetic is supposed that respects Butler - Volmer equation. Far from equilibrium, anodic reactions could be neglected. A Tafel modified expression describes the electrochemical reactions rate on surface and is adapted to calculate the partial current. For example, on the first step of deposition reaction on nickel substrate, partial current density,  $i_{11}$ , could be wrote as:

$$i_{11} = -Fk_{11}^{0}C_{Ni}^{2+}\theta_{Ni}(1-\theta_{1}-\theta_{2}-\theta_{3})exp(-b_{11}\eta_{11})$$

### 2.8. Software for predictive calculus of zincnickel alloy composition

To simulate zinc-nickel alloy deposition, it was elaborated a soft-ware, which uses the calculus relationship from described mathematic model. The calculus stops when difference between a calculated value and a previos one is smaller than  $10^{-5}$ .

The program lines are written as follows:

using System;

using System.Collections.Generic; using System.ComponentModel; using System.Data; using System.Drawing; using System.Text; using System.Windows.Forms;

```
namespace CalculTETAi
{
    public partial class frmMain : Form
    {
        public frmMain()
        {
        InitializeComponent();
    }
```

double F, Ki0, Bi, EtaI, C0, ITotal, Ai, t, TetaS, CH, CNi, CZn, TetaIInitial, TetaZn, TetaNi; double TetaICalculat; double Ci, Ii; private void m\_btnCalculeaza\_Click( object sender, EventArgs e)

```
{
          m_tbTetaICalculat.Text = "";
          try
            F = double.Parse( m_tbF.Text );
            Ki0 = double.Parse( m tbKi0.Text );
            Bi = double.Parse( m_tbBi.Text );
            EtaI = double.Parse( m tbEtaI.Text );
            C0 = double.Parse( m tbC0.Text );
            ITotal
                                    double.Parse(
                          =
m_tbITotal.Text );
            Ai = double.Parse( m_tbAi.Text );
            t = double.Parse( m_tbT.Text );
            TetaS
                                    double.Parse(
                          =
m_tbTetaS.Text );
            CH = double.Parse( m tbCH.Text );
            CNi = double.Parse( m_tbCNi.Text );
            CZn = double.Parse(m tbCZn.Text
);
            TetaIInitial
                                    double.Parse(
                             =
m_tbTetaIInitial.Text );
            TetaZn
                                    double.Parse(
m tbTetaZn.Text );
            TetaNi
                                    double.Parse(
                           =
m_tbTetaNi.Text );
          }
          catch
```

MessageBox.Show( "Introduceti valori corecte", "Atentie", MessageBoxButtons.OK, MessageBoxIcon.Warning );

return; } int Contor = 0; int NumarBucle = 1000;TetaICalculat = TetaIInitial; do { TetaIInitial = TetaICalculat; Ci = C0 \* Math.Exp(-Ki0 \* Ai \* t);Ii = -F \* Ki0 \* CNi \* CZn \* CH \* TetaZn \* TetaNi \* (1 - TetaIInitial - TetaS) \* Math.Exp( -Bi \* EtaI ); TetaICalculat = Ii / ITotal; Contor++: if( Contor > NumarBucle ) break; while( Math.Abs( TetaIInitial -} TetaICalculat ) > 1 \* Math.Pow(10, -5)); if( Contor > NumarBucle ) MessageBox.Show( "S-a depasit numarul de bucle!". "Atentie", MessageBoxButtons.OK, MessageBoxIcon.Warning ); else { m\_tbTetaICalculat.Text \_ TetaICalculat.ToString(); } }

private void m\_btnIesire\_Click( object sender, EventArgs e )

{

this.Close();

Ni-Zn-COMP	_ 8 ×
F	96500
$k_i^0$	
$b_i$	
$\eta_i$	
C(0)	
i <sub>total</sub>	
$A_{i}$	
t	
$\theta_z$	
$C_{H}$	
$C_{Ni}^{2+}$	
$C_{Zn}^{2+}$	
$\theta_{iinit}$	0.5
$\theta_{Zn}$	0.5
$\theta_{Ni}$	0.5
$\theta_{i \ calc}$	
Calculeaza	Iesire

Figure 3. User interface with the software for calculus of alloy composition

### **3. CONCLUSIONS**

This model establishes a mathematic apparatus to describe zinc-nickel alloy co-deposition processes, using the substrate effect model for different concentration of electrolyte and for different applied potentials. There was a good correlation between experimental data and the prediction of this model.

### 4. ACKNOWLEDGMENTS

This paper was supported by the project "Progress and development through post-doctoral research and innovation in engineering and applied sciences- PRiDE - Contract no. POSDRU/89/1.5/S/57083", project co-funded from European Social Fund through Sectorial Operational Program Human Resources 2007-2013.

#### **5. REFERENCES**

- [1]. Bard, A.J., *Electrochemical Methods. Fundamentals and Applications*, John Wiley and Sons, New-York, 2001
- [2]. Di Bari,G.A., Modern Electroplating, Fourth Edition, Edited by Mordechay Schlesinger and Milan Paunovic, John Wiley & Song, Inc., 2000
- [3]. Teeratananon, M., Saidi, K., Fenouillet, B., Vergnes, H., *Journnes d'electrochimic*, Poiters, France, june 2008
- [4]. Matlosz, M., Journal Electrochemistry Soc., 140(1993)2272
- [5]. Soares, M.E., Souza, C.A.C., Kuri, S.E., Corrosion resitence of Zn-Ni electrodeposited alloy obtained with a controlled electrolyte flow and gelatin additive, Science Direct, vol.201, Issue 6, dec.2006, p.2953-2959
- [6]. Schlesinger, M., *Electrodeposition of Alloys*, Modern Electroplating, Fourth Edition, John Wiley and Sons, Inc. New-York, 2000
- [7] Brenner A, Electrodeposition of Alloys, Vol.I, Academic Press, New York, 1963
- [8]. Vasilache, V., Gutt, Gh., Vasilache, T., Rev. Chim. (Bucuresti), 59, nr.8, 2008, p. 915
- [9]. Vasilache, V., Ph. D. Thesis, University Stefan cel Mare of Suceava, 2008
- [10]. Vasilache V., Gutt Gh. Vasilache T., Studies about electrochemical plating with zinc-nickel alloys. The influence of potential through stoichiometric composition, Revista de Chimie, Bucureşti, vol.59,nr.9 (2008)
- [11] Vasilache V, Gutt S, Gutt Gh, Vasilache Tr, Sandu I, Sandu IG. Determination of the Dimension of Crystalline Grains of Thin Layers of Zinc-Nickel Alloys Electrochemically Deposited. Metalurgia International, 2009, 14: 49-53;